

INDUSTRIAL Wastewater

December 2008/January 2009

Volume 7, Number 6

Easy Upgrade

A membrane bioreactor enables a meat processor to upgrade its wastewater treatment system with little fuss

Ralph Teckenberg, Sandra Schuler, Andreas Böhm, Torsten Hackner, and Markus Roediger

Hans Kupfer & Sohn GmbH & Co. KG (Heilsbronn, Germany), a large meat processor in the German state of Bavaria, had an onsite wastewater treatment system that included mechanical screening, flotation, and biological treatment. The company had expanded its production facilities over the years but not the treatment system. Eventually, the system began repeatedly exceeding its discharge limits. Furthermore, the effluent is discharged into a small creek that can barely handle peak loads.

The company hired a project team to plan a new, state-of-the-art wastewater treatment system. The team selected a membrane bioreactor (MBR) because it has a small footprint, removes 100% of suspended solids, and provides reusable effluent.

Treatment System Design

The project team designed the pilot-test system to handle a maximum feed rate of 2.5 m³/h (660 gal/h). Because of the wastewater's high grease content, the team decided to install a dissolved-air flotation (DAF) unit upstream of the MBR. So, the treatment train includes a settling tank with scumboard, a 2-m³ (528-gal) pump and holding tank, a DAF unit with chemical treatment, a second 2-m³ (528-gal) pump and holding tank, and an MBR.

The settling tank and scumboard remove coarse material, such as sausages and meat pieces, from wastewater. The DAF unit removes free and emulsified grease from wastewater. Treatment chemicals, such as iron chloride and polymer, enhance grease separation.

The vacuum rotation MBR pro-

vides both carbon degradation and nitrification. (Denitrification was omitted during this test.) During testing, the aeration tank contained 8000 to 12,000 mg/L of mixed liquor suspended solids (MLSS), while the filtration chamber contained 12,000 to 16,000 mg/L of MLSS (an aeration-to-filtration MLSS ratio of 2:3). The 12-m³ (3170-gal) membrane chamber provided a membrane surface area of 108 m² (1163 ft²). Flow rates varied from 0.5 to 2.5 m³/h (132 to 66 gal/h), corresponding to membrane flux rates of 0.12 to 0.48 m³/m²·d (2.9 to 11.8 gal/ft²·d).

Vacuum Rotation Membrane

Membrane filters use a pressure differential to remove suspended solids from water. The pressure forces or draws water through the membrane while leaving solids, bacteria, and even most viruses behind. The amount of pressure needed depends on membrane quality and pore size.

In a vacuum rotation membrane (VRM[®]) bioreactor system, the membranes are installed in separate chambers after the aeration tanks. Trapezoidal ultrafiltration-membrane plates are installed in parallel on a rotating drum sup-

ported on a frame (see Figure 1, p. 2, and Figure 2, p. 3). Each plate also is connected to a permeate-discharge hose that leads to a permeate-collection pipe. The pipes are guided onto a special support from where permeate is discharged.

The overflows required to keep the ultrafiltration membranes operating are achieved via airflow in the bioreactor.

Wastewater Parameters

Before starting pilot tests, the project team collected 24-hour composite samples of the wastewater and analyzed them for pH, chemical oxygen demand (COD), ammonia-nitrogen, nitrate-nitrogen, and phosphate-phosphorus (see Table 1, p. 3). The team also collected grab samples to determine biochemical oxygen demand (BOD) and, therefore, evaluate

Continued on page 2

Algal Biofuel Industry May Need Wastewater To Prosper

As entrepreneurs rush to meet the growing demand for renewable fuel sources, many have focused on algae. The lowly plant material grows quickly, can be raised on marginal land, and produces oil that can be converted into biofuel. Observers acknowledge that wastewater from industrial, municipal, and agricultural sources could play a key role in the development of this potential fuel source. Such a partnership would provide the nascent biofuel industry with a

Continued on page 6

In This Issue

Newspaper-Based Gel Shows Promise in Removing Gold From Wastewater.....	5
Troubleshooting Membrane Bioreactor Failures.....	8
Briefs.....	14

INDUSTRIAL Wastewater

EDITOR **LaShell Stratton**

CONTRIBUTING EDITORS

Laura Bridgewater, Jay Landers

EDITORIAL ASSISTANT **Margaret Richards**

PRODUCTION MANAGER **Laura J. Leslie**

PUBLISHER **William J. Bertera**

EDITORIAL ADVISORY BOARD:

CHAIR: **David Russell**

Global Environmental Operations (Lilburn, Ga.)

David Beecher

Kodak Co. (Rochester, N.Y.)

Kamesh Gupta

General Motors (Detroit, Mich.)

Ken Wood

Dupont Co. (Wilmington, Del.)

Mark Wyzalek

Macon Water Authority (Macon, Ga.)

The Editorial Advisory Board does not necessarily approve, disapprove, or endorse the contents of *Industrial Wastewater*.

Editorial Offices:

Water Environment Federation

601 Wythe St.

Alexandria, VA 22314-1994

Telephone: (703) 684-2400

Fax: (703) 684-2492



PRESIDENT: **Rebecca West**

PRESIDENT-ELECT: **Paul Freedman**

VICE PRESIDENT: **Jeanette Brown**

TREASURER: **Chuck Weir**

PAST PRESIDENT: **Adam Zabinski**

EXECUTIVE DIRECTOR: **William J. Bertera**

Industrial Wastewater (ISSN 1067-5337) is published 6 times/yr. ©2008 by the Water Environment Federation, 601 Wythe St., Alexandria, VA 22314 USA; (703) 684-2400.

Subscriptions are \$129/yr. (\$89: WEF members). Single copy price is \$22 (\$18: WEF Members). Editorial correspondence should be sent to the Editor. Send change of address (8 weeks advance notice) and claims for missing issues to pubs@wef.org.

Bulk reprinting of articles prohibited.

The Water Environment Federation assumes no responsibility for opinions or statements of fact expressed by contributors or staff, and articles do not necessarily represent official organization policy.

www.wef.org

Technical Innovation in Water Quality

Notice to Subscribers

Beginning with the February/March 2009 issue, *Industrial Wastewater* is moving to an electronic-only format. When each issue is published, you will receive an e-mail notification with a link to the *Industrial Wastewater* Web site, where you will be able to print and download the issue in PDF format. Subscribers will be able to access current issues and archives at www.wef.org/IndustrialWastewater. The print edition you currently receive will no longer be available.

To ensure that you continue to receive *Industrial Wastewater* without interruption, we encourage you to update your e-mail address at www.wef.org/MembershipCareers/MembershipInformation/RenewModifyMembership, or by contacting WEF Customer Service at csc@wef.org, (800) 666-0206 (within the United States and Canada), or (703) 684-2452.

Easy Upgrade Continued from page 1

the wastewater's biodegradability (via the ratio of COD to BOD). A COD:BOD of 2.0 or more generally indicates that the wastewater will not biodegrade easily. The ratio for this facility's wastewater ranged from 1.8 to 2.2. The team attributed the higher ratios to the wastewater's relatively high grease content.

Pilot-Test Results

In general, pilot tests showed that an MBR requires an adequate pretreatment or solids-treatment system. Iron-chloride additions in the DAF cut total phospho-

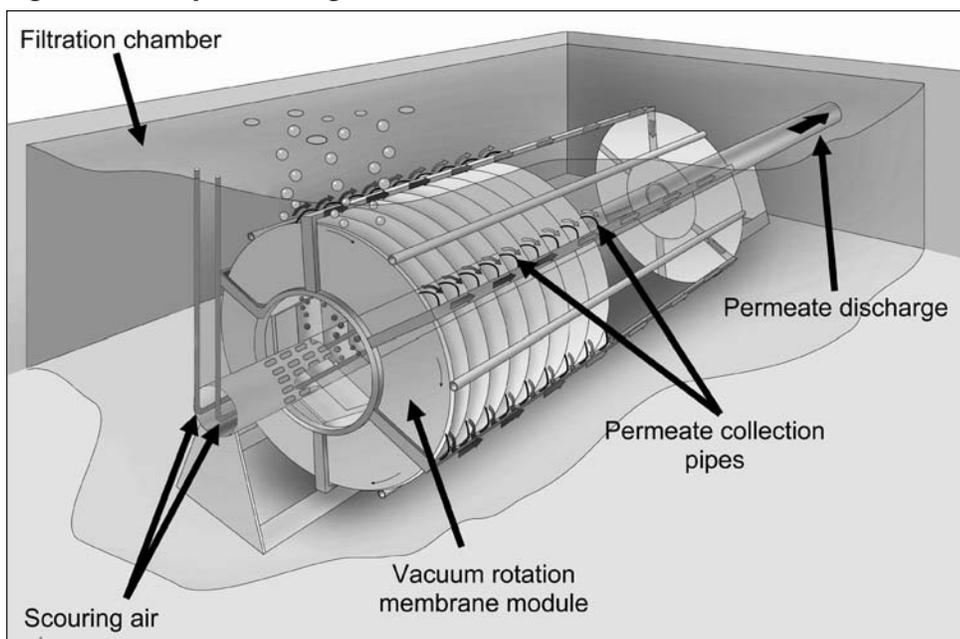
rus from 20 to 9.8 mg/L, on average (a 54% reduction).

DAF cut the average COD from between 1800 and 2000 mg/L down to 1000 to 1200 mg/L. This shifted the COD:BOD closer to 2, thereby reducing clarification costs and increasing treatment stability. The good solids properties also ensured better filterability, thereby increasing membrane flux.

However, DAF had virtually no effect on ammonium concentrations, which ranged from 5 to 7 mg/L.

Transmembrane pressure and flux indicate that DAF pretreatment improved MLSS and filterability. The pilot test also showed that

Figure 1. Principle Drawing of a Vacuum Rotation Membrane Unit

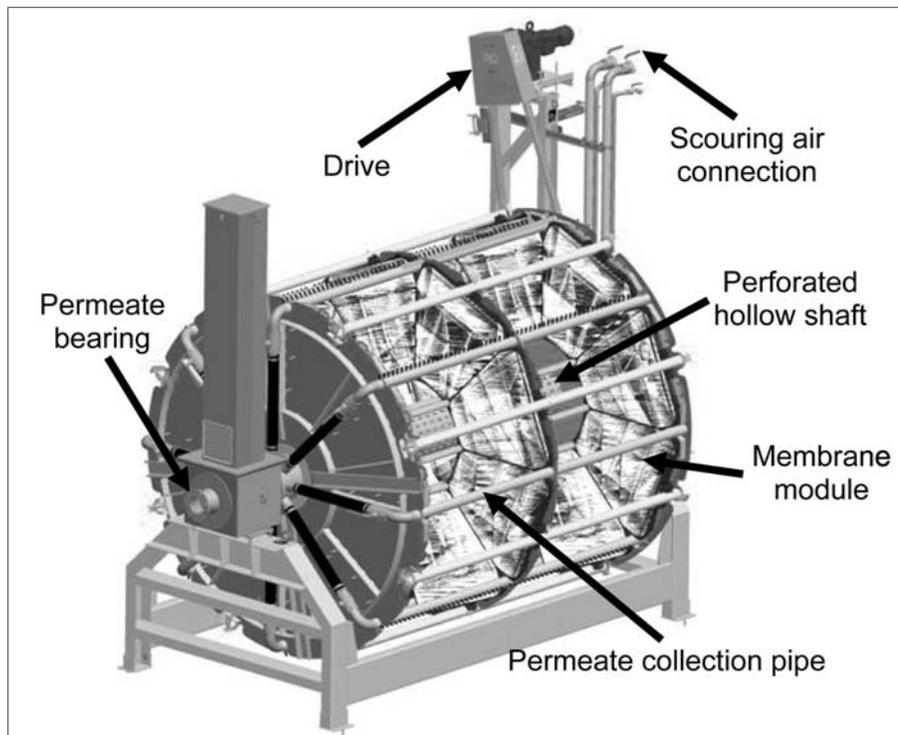


HANS HUBER AG

Table 1. Wastewater Parameters

	Chemical oxygen demand (mg/L)	Ammonia–nitrogen (mg/L)	Nitrate–nitrogen (mg/L)	Phosphate–phosphorus (mg/L)	pH
Minimum	675	2.12	1.27	10.11	7.67
Maximum	5517	10.44	7.13	34.25	10.53
Average	1741	5.3	4.48	19.57	9.13
85th percentile	2050	5.8	6.4	18.0	9.8

Figure 2. Detailed Drawing of a Vacuum Rotation Membrane Unit



a low flux ensures process stability with only a few extra scouring sequences and prolonged cleaning intervals.

After startup and optimization, the operating parameters for layout and process design of the full-scale plant and expected discharge concentrations could be determined.

The MBR's COD reduction was

always more than 97%. Because of this excellent performance, effluent COD averaged 20 mg/L. In the permeate, ammonia averaged 0.66 mg/L. COD and ammonia–nitrogen levels indicated that nitrification was stable, with good results. Phosphorus removal was mainly achieved in the DAF unit, but the MBR cut total phosphorus to 3.1 mg/L, on average.

Table 2. Permeate Quality

	Chemical oxygen demand (mg/L)	Ammonia–nitrogen (mg/L)	Total phosphorus (mg/L)	Total nitrogen (mg/L)
Required discharge values	75.0	5.0	2	18
Permeate (average)	22.82	0.57	0.1	4.75

Full-Scale Design

The full-scale wastewater treatment system was designed for an average daily flow of 1200 m³/d (317,000 gal/d) and a maximum flow of 1600 m³/d (423,000 gal/d). Temporary peak flows of up to 4800 m³/d (1.27 mgd) may occur. A 1500-m³ (396,000-gal) equalization tank, however, ensures that peak hourly flow does not exceed 2400 m³/d (634,000 gal/d) during normal operations.

The new system includes coarse screening (a 15-mm multirake bar screen), fine screening (a 1-mm wedgewire rotating drum screen), an equalization tank, a 1.7-m³/min (440-gal/min) DAF unit with chemical addition, and an MBR.

The pretreatment system reduces COD by 50% via extensive removal of fats, oils, and grease. The following aeration stage is designed for 1920 kg/d of COD and extensive nitrogen reduction. A three-line submerged membrane filtration plant with an average flux rate of 0.3 m³/m²·d (7.1 gal/ft²·d) is installed downstream of the 900-m³ (240,000-gal) aeration tank, which operates with intermittent aeration. Each of the three membrane tanks contains one VRM unit (VRM 30/400) with an active membrane surface area of 2400 m² (26,000 ft²) per unit.

Phosphorus is removed at two points in the system: the pipe flocculator before the DAF unit, and the biological treatment step. As expected, DAF reduces phosphorus by about 50%, on average. The aeration basin removes more phosphorus via simultaneous precipitation with iron chloride.

Waste activated sludge from the aeration stage is mechanically prethickened and, along with DAF sludge and screenings, trucked to a local biogas

HANS HUBER AG



HANS HUBER AG

The pretreatment processes for the vacuum rotation membrane unit installed at a German meat processing facility include fine screens and a dissolved air flotation unit.

plant. This cost-effective disposal method is possible because it does not include sanitary wastes.

Because of its excellent quality, the permeate can be reused as service water for vapor generation or fed into the onsite storage pond for fire protection.

Excellent Results

In January 2008, the project team seeded the MBR with activated sludge from two nearby wastewater treatment plants. Extra flow from a new production line and additional nutrients soon increased MLSS to the design concentra-

tion of 8000 mg/L.

After initial startup, the full-scale MBR has consistently complied with all discharge requirements. Since March 2008, the MBR plant has consistently met its permitted limits and has since begun discharging directly into the creek.

However, the permeate meets reuse quality standards (see Table 2, p. 3; the table shows effluent quality and permitted discharge limits, not reuse standards). COD averages about 20 mg/L, which is considerably less than the required permit value (75 mg/L).

Likewise, ammonia, nitrogen, and phosphorus are well within limits. Also, the permeate is free of suspended solids — the main reason why it is suitable for reuse.

MBRs provide constant high treatment efficiency and can significantly reduce the footprint and number of treatment steps required. This is especially useful for industrial applications, where land is at a premium and water can be reused onsite.

Ralph Teckenberg is head of the Industrial Department at Hans Huber AG (Berching, Germany). Sandra Schuler is a membrane bioreactor process engineer at Huber Technology Inc. (Huntersville, N.C.). Andreas Böhm is an industrial sales engineer and Torsten Hackner is head of the Filtration and Reuse Department and VRM product manager at Hans Huber AG. Markus Roediger is an independent consulting engineer for wastewater technology in Stuttgart, Germany.



HANS HUBER AG

From the top of the vacuum rotation membrane's filtration tank, it is obvious whether the unit's air scouring is on (left) or off (right).